

AMENDMENTS TO THE CLAIMS

Claim 1 (Currently Amended): A process for preparing trichlorosilan (HSiCl_3) by catalytic hydrodehalogenation of silicon tetrachloride (SiCl_4) in the presence of hydrogen and a supported catalyst at a temperature in the range from 300 to 1000°C, wherein said catalytic hydrodehalogenation comprises contacting said supported catalyst with a SiCl_4/H_2 mixture having a molar ratio of from 1:0.9 to 1:20,

wherein said supported catalyst has a catalyst content, calculated as element, of from 0.1 to 10% by weight and comprises at least one metal or metal salt selected from the group consisting of calcium, strontium, barium, calcium chloride, strontium chloride, and barium chloride, and

wherein said at least one metal or metal salt has been applied to a support selected from the group consisting of leached glass, fused silica, a porous siliceous support and a SiO_2 support,

wherein said catalytic hydrodehalogenation is conducted in a fixed-bed reactor, in a fluidized-bed reactor or in a moving-bed reactor, and

wherein said catalytic hydrodehalogenation is conducted at a temperature in the range from 600 to 950°C and a pressure of from 0.1 to 100 bar abs.

Claims 2-4 (Canceled)

Claim 5 (Currently Amended): The process as claimed in claim 1,
wherein the supported catalyst used has a catalyst content, calculated as element, of from 0.1 to 10% 1 to 8% by weight.

Claim 6 (Currently Amended): The process as claimed in claim 1,
wherein [[an]] said catalytic hydrodehalogenation comprises contacting said
supported catalyst with a SiCl₄/H₂ mixture having a molar ratio of from 1:0.9 to 1:20 1:1 to
1:10 is brought into contact with the catalyst.

Claim 7 (Currently Amended): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation is conducted the reaction is carried out in
a fixed-bed reactor, ~~in a fluidized bed reactor or in a moving bed reactor.~~

Claim 8 (Currently Amended): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation is conducted the catalytic reaction is
~~carried out at a temperature in the range from 700 to 900°C 600 to 950°C and a pressure of~~
~~from 0.1 to 100 bar abs.~~

Claim 9 (Currently Amended): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation is conducted the catalytic reaction is
~~carried out at a space velocity of from 2000 to 30000 h⁻¹ and the gas stream has a linear~~
velocity of from 0.01 to 10 m/s in the reactor.

Claim 10 (Previously Presented): The process as claimed in claim 1,
wherein HSiCl₃ is isolated from the product mixture or the product mixture is used
further directly.

Claim 11 (New): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation comprises contacting said supported catalyst with a SiCl₄/H₂ mixture having a molar ratio of from 1:1.5 to 1:8.

Claim 12 (New): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation comprises contacting said supported catalyst with a SiCl₄/H₂ mixture having a molar ratio of from 1:2 to 1:4.

Claim 13 (New): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation is conducted in a fluidized-bed reactor.

Claim 14 (New): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation is conducted in a moving-bed reactor.

Claim 15 (New): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation is conducted at a pressure of from 1 to 10 bar abs.

Claim 16 (New): The process as claimed in claim 1,
wherein said catalytic hydrodehalogenation is conducted at a pressure of from 1.5 to 2.5 bar abs.

Claim 17 (New): The process as claimed in claim 9,
wherein said catalytic hydrodehalogenation is conducted at a space velocity of from 5 000 to 15 000 h⁻¹.

Claim 18 (New): The process as claimed in claim 9,
wherein said gas stream has a linear velocity of from 0.02 to 8 m/s in the reactor.

Claim 19 (New): The process as claimed in claim 9,
wherein said gas stream has a linear velocity of from 0.03 to 5 m/s in the reactor.